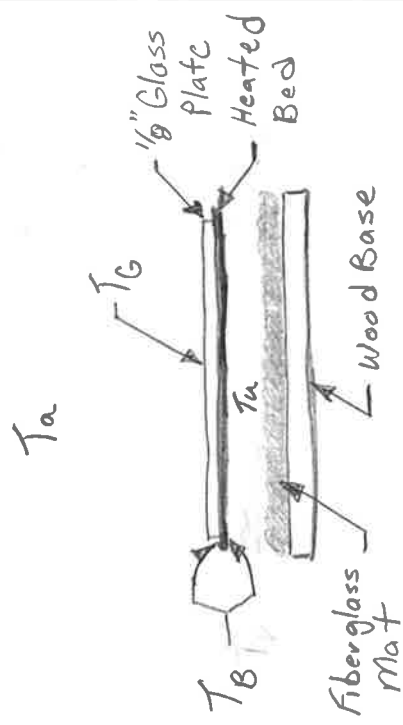
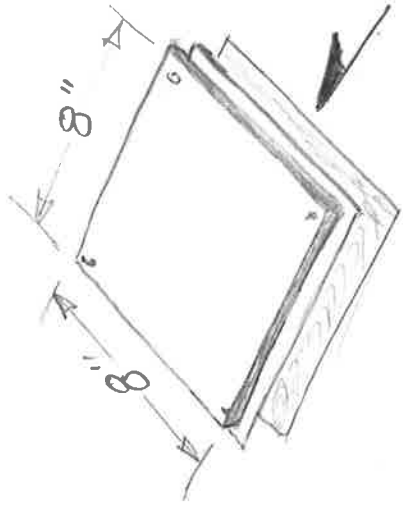


①



T_a - temp Ambient in box

T_G - temp at glass surface

T_B - temp of Bed, thermistor reading

T_u - temp under bed

Above plate

Overall temp change $T_B - T_a$

Steady state heat transfer for flat plate

$$q = \frac{BT_u}{hr} = \frac{kA\Delta T}{\Delta x}, k - \text{thermal cond.}, A - \text{plate area}, \Delta T - \text{temp change}$$

Δx - plate thickness

$q_G = \frac{k_g A (T_B - T_G)}{\Delta x_G}$; Heat Transfer rate through glass

Radiation + convection from glass plate

$$q_{a+c} = h_a A (T_G - T_a)$$

$$q_G = q_{a+c} \Rightarrow \frac{k_g A (T_B - T_G)}{\Delta x_G} = h_a A (T_G - T_a)$$

$$k_g T_B - k_g T_G = \Delta x_G h_a T_G - \Delta x_G h_a T_a$$

$$k_g T_B + \Delta x_G h_a T_a = \Delta x_G h_a T_G + k_g T_G$$

$$k_g T_B + \Delta x_G h_a T_a = T_G (\Delta x_G h_a + k_g)$$

$$T_G = \frac{k_g T_B + \Delta x_G h_a T_a}{\Delta x_G h_a + k_g}$$

②

$$k_g = 0.455 \text{ BTU/hr} \cdot \text{ft}^2 (\text{°F}/\text{ft})$$

$$T_B = 110^\circ\text{C} = 230^\circ\text{F}$$

$$T_a = 80^\circ\text{F}$$

$$\Delta X_G = 0.125 \text{ in} = 0.0104 \text{ ft}$$

$$h_a = 2.7 \text{ BTU/hr} \cdot \text{ft}^2 \cdot \text{°F}$$

$$T_G = \frac{(0.455 \text{ BTU/hr} \cdot \text{ft}^2)(230^\circ\text{F}) + (0.0104 \text{ ft})(2.7 \text{ BTU/hr} \cdot \text{ft}^2 \cdot \text{°F})(80^\circ\text{F})}{(0.0104 \text{ ft})(2.7 \text{ BTU/hr} \cdot \text{ft}^2 \cdot \text{°F}) + 0.455 \text{ BTU/hr} \cdot \text{ft}^2 \cdot \text{°F}/\text{ft}}$$

$$\frac{\text{BTU} \cdot \text{ft}}{\text{hr} \cdot \text{ft}^2}$$

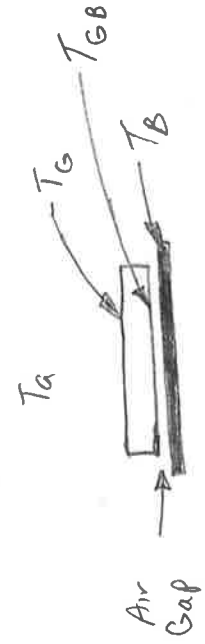
$$\frac{(0.455)(230) + (0.0104)(2.7)(80)}{(0.0104)(2.7) + 0.455}$$

$$\frac{104.65 + 2.2464}{0.02808 + 0.455}$$

$$\frac{106.8964}{0.48308} \text{ °F}$$

$$\frac{106.8964}{0.48308} = 221.3^\circ\text{F} = 105^\circ\text{C}$$

③



T_{GB} = temp at glass bottom ; ΔX_{Gap} = air gap between bed
 $Q = \frac{k_{air} A (T_B - T_{GB})}{\Delta X_{Gap}} = \frac{k_g A (T_{GB} - T_G)}{\Delta X_G} = h_a A (T_G - T_a)$ d glass

from the prior calc :

$$T_G = \frac{k_g T_{GB} + \Delta X_G h_a T_a}{\Delta X_G h_a + k_g} \quad (1)$$

we don't know T_{GB} so we need another equation

$$\frac{k_{air} A (T_B - T_{GB})}{\Delta X_{Gap}} = \frac{k_g A (T_{GB} - T_G)}{\Delta X_G}$$

$$k_{air} (T_B - T_{GB}) = \frac{\Delta X_{Gap}}{\Delta X_G} k_g (T_{GB} - T_G)$$

$$k_{air} T_B - k_{air} T_{GB} = \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_{GB} - \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G$$

$$k_{air} T_B + \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G = \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_{GB} + k_{air} T_{GB}$$

$$k_{air} T_B + \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G = \left[\frac{\Delta X_{Gap}}{\Delta X_G} k_g + k_{air} \right] T_{GB}$$

$$T_{GB} = 1 / \left[\frac{\Delta X_{Gap}}{\Delta X_G} k_g + k_{air} \right] \left\{ k_{air} T_B + \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G \right\} \quad (2)$$

$$\text{Let } C = 1 / \left[\frac{\Delta X_{Gap}}{\Delta X_G} k_g + k_{air} \right]$$

Sub (2) in to (1)

$$T_G = \frac{k_g \left[C \cdot (k_{air} T_B + \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G) \right] + \Delta X_G h_a T_a}{\Delta X_G h_a + k_g}$$

$$T_G = \frac{k_g C k_{air} T_B + k_g C \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G + \Delta X_G h_a T_a}{\Delta X_G h_a + k_g}$$

$$D = \Delta X_G h_a + k_g$$

④

$$T_G = \frac{k_g C k_{air} T_B + k_g C \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G + \Delta X_G h_a T_a}{D}$$

$$T_G - k_g \frac{C}{D} \frac{\Delta X_{Gap}}{\Delta X_G} k_g T_G = k_g \frac{C}{D} k_{air} T_B + \frac{\Delta X_G}{D} h_a T_a$$

$$T_G = \frac{k_g \frac{C}{D} k_{air} T_B + \frac{\Delta X_G}{D} h_a T_a}{1 - k_g \frac{C}{D} \frac{\Delta X_{Gap}}{\Delta X_G} k_g}$$

(5)

$$k_g = 0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}$$

$$T_B = 110^\circ\text{C} = 230^\circ\text{F}$$

$$T_a = 80^\circ\text{F}$$

$$\Delta X_G = 0.125 \text{ in} = 0.0104 \text{ ft}$$

$$h_a = 2.7 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot ^\circ\text{F}}$$

$$\Delta X_{\text{Gap}} = 0.5 \text{ mm} = 0.00164 \text{ ft}$$

$$k_{\text{air}} = 0.0183 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}$$

$$C = \frac{1}{\left[\frac{(0.00164 \text{ ft})}{(0.0104 \text{ ft})} (0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}) + 0.0183 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})} \right]}$$

$$C = 11.1049 \frac{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}{\text{BTU}}$$

$$D = (0.0104 \text{ ft}) (2.7 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot ^\circ\text{F}}) + 0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}$$

$$D = 0.48308 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}$$

$$k_g \frac{C}{D} k_{\text{air}} T_B = (0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}) \frac{11.1049 \frac{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}{\text{BTU}}}{0.48308 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}} - (0.0183 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}) \times 230^\circ\text{F}$$

$$k_g \frac{C}{D} k_{\text{air}} T_B = 44.024^\circ\text{F}$$

$$\frac{\Delta X_G}{D} h_a T_a = \frac{(0.0104 \text{ ft})}{0.48308 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}} (2.7 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot ^\circ\text{F}}) (80^\circ\text{F})$$

$$\frac{\Delta X_G}{D} h_a T_a = 4.65^\circ\text{F}$$

$$k_g \frac{C}{D} \frac{\Delta X_{\text{Gap}}}{\Delta G_G} k_g = (0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}) \frac{11.1049 \frac{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}{\text{BTU}}}{0.48308 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}} (0.455 \frac{\text{BTU}}{\text{hr} \cdot \text{ft}^2 \cdot (^\circ\text{F}/\text{ft})}) \frac{0.00164}{0.0104}$$

$$= 0.75$$

$$T_G = \frac{44.024^\circ\text{F} + 4.65^\circ\text{F}}{1 - 0.75} = \underline{\underline{90.4^\circ\text{C}}}$$